

Achieving Continuous Manufacturing for Final Dosage Formation: Challenges and How to Meet Them

May 20-21, 2014 Continuous Symposium

Stephen Byrn*, Maricio Futran**, Hayden Thomas***, Eric Jayjock**, Nicola Maron†, Robert F. Meyer††, Allan S. Myerson†††, Michael P. Thien††, and Bernhardt L. Trout†††

* Department of Industrial and Physical Pharmacy, Purdue University

**Janssen Supply Group, LLC

***Vertex Pharmaceuticals, Inc.

† I.M.A. Industria Macchine Automatiche S.p.A.

†† Global Science, Technology and Commercialization; Merck Manufacturing Division; Merck & Co., Inc.

††† Department of Chemical Engineering, Massachusetts Institute of Technology and Novartis-MIT Center for Continuous Manufacturing

Executive Summary

We describe the key issues and possibilities for continuous final dosage formation, otherwise known as downstream processing or drug product manufacturing. A distinction is made between heterogeneous processing and homogeneous processing, the latter of which is expected to add more value to continuous manufacturing. We also give the key motivations for moving to continuous manufacturing, some of the exciting new technologies, and the barriers to implementation of continuous manufacturing.

Continuous processing of heterogeneous blends is the natural first step in converting existing batch processes to continuous. In heterogeneous processing, there are discrete particles that can segregate, versus in homogeneous processing, components are blended and homogenized such that they do not segregate. Heterogeneous processing can incorporate technologies that are closer to existing technologies, where homogeneous processing necessitates the development and incorporation of new technologies. Homogeneous processing has the greatest potential for reaping the full rewards of continuous manufacturing, but it takes long-term vision and a more significant change in process development than heterogeneous processing. Heterogeneous processing has the detriment that, since the technologies are adopted rather than developed, there is a strong tendency to incorporate correction steps, what we call below ‘The Rube Goldberg Problem.’ Thus, although heterogeneous processing will likely play a major role in the near-term transformation of heterogeneous to continuous processing, it is expected that homogeneous processing is the next step that will follow.

Specific action items for industry leaders are:

- Form pre-competitive partnerships, including industry (pharmaceutical companies and equipment manufacturers), government, and universities. These pre-competitive partnerships would develop case studies of continuous manufacturing and ideally perform joint-technology development, including development of small-scale equipment and processes.
- Develop ways to invest internally in continuous manufacturing. How best to do this will depend on the specifics of a given organization, in particular the current development projects. Upper managers will need to energize their process developers to incorporate continuous manufacturing in at least part of their processes to gain experience and demonstrate directly the benefits.

- 49 • Training of continuous manufacturing technologies, organizational approaches, and regulatory
50 approaches is a key area that industrial leaders should pursue together.
51

52 Keywords: upstream, downstream, drug substance, drug product, mixing, solution, dispersion,
53 heterogeneous, homogeneous

54 **1. Introduction to Continuous Manufacturing for Final Dosage Formation**

55
56 As discussed in the Introduction of this volume, ‘continuous manufacturing’ means integration, a
57 systems approach, and a model-based control within a flow process. Thus, since a continuous
58 process is designed as a whole, the distinction between upstream and downstream, or drug
59 substance and drug product, as currently used, can be, potentially, eliminated. The disappearance of
60 these terms corresponds to a change in mindset, which itself would lead to the adoption of new
61 terms. There is, however, clearly still the need for expertise in chemical synthesis, reaction
62 engineering and work-up on the one hand, and material understanding, formulation development,
63 and formulation process engineering on the other. Here we focus on final dosage formation,
64 including in this analysis the overlap between it and chemical synthesis, reaction engineering, and
65 work-up. While we cannot with certainty predict which technologies and technology strategies
66 pharmaceutical manufacturers will adopt in the future, we do believe that the future can be very
67 different than the current approach, and herein we outline the vision of continuous manufacturing
68 for final dosage formation, the barriers to achieving that vision, and how the industry should work to
69 overcome those barriers.

70
71 While the technologies, and therefore development and manufacturing expertise, needed for the final
72 dosage formulation aspects of continuous processing are different than those needed for chemical
73 synthesis, reaction engineering, and work-up, there are many areas of overlap. These include
74 crystallization, powder handling, solvents processing, process safety, and process monitoring and
75 control technologies. In fact, as continuous manufacturing becomes more and more prevalent and
76 new technologies come about, we expect that the various development and manufacturing specialties
77 will tend towards convergence. There will still be various areas of expertise, but specialists will need
78 to interact with other specialists much more than they do presently, in order to coordinate process
79 development, and the differentiation among process development teams will become smaller and
80 smaller. For example, the solvents for chemistry development will need to be chosen to take into
81 account work-up, in addition to, at least for the last chemical step, processing aspects of final dosage
82 formation, such as drying and mechanical properties. Furthermore, while we expect a transition
83 period during which batch technologies are converted to similar flow technologies in which there
84 will still be substantial in-process powder handling such that actives and excipients are processed
85 heterogeneously, in the long run we expect that the advantages of homogeneous processing will be
86 such that most, if not all, continuous processes will involve homogenous processing technologies, in
87 which actives and excipients are processed together. Homogeneous processing will necessitate new
88 approaches to final dosage formation and corresponding new technologies, all of which will need to
89 be integrated tightly with the other aspects of the process.

90
91 For these reasons, we term the subject of this white paper ‘final dosage formation,’ keeping in mind
92 that in the world of continuous manufacturing terms like ‘upstream,’ ‘downstream,’ ‘drug substance’
93 and ‘drug product’ could be considered transitional terms, and may very well disappear. The focus
94 here is on formation of tablets for oral dosage, but the reader will readily see how the approaches
95 below can be used to produce alternative dosage forms, including films, liquids, depots, inserts and
96 implants.

97 **2. How the Vision of Continuous Pharmaceutical Manufacturing will Change Final Dosage**
98 **Form Operations**
99

100 Given that continuous manufacturing encompasses integration, a systems approach, flow, and model-
101 based control, future continuous facilities will be set up quite differently than existing facilities.
102 Below, we discuss the trade-offs involved in dedicated final dosage form process trains versus multi-
103 use process trains. We do envision minimizing, if not eliminating, powders handling, at least within
104 the process itself—there will, most likely, still be the need for powder dosage into the process. In
105 addition, even if processes do not achieve full continuous manufacturing as we have defined it, steps
106 in that direction should prove to be of significant benefit across the industry, from brand Pharma
107 companies to generics, from small-scale production to large-scale production, and from simple to
108 complex formulations. Integration within a systems approach itself leads to a reduction of process
109 steps, as the number of ‘correction’ steps can be reduced or eliminated and in general processing
110 steps can be streamlined. In batch processes, actives are almost always formed upstream into
111 powders that typically do not have the properties needed for downstream. Thus, initial downstream
112 steps typically include milling and blending. These can be streamlined in a continuous process.
113 Furthermore, batch downstream steps often include granulation so that the mixture will have the
114 properties needed for further processing, which is necessary because the mixture does not
115 inherently possess the desired properties. Given that continuous manufacturing naturally
116 encompasses more up front understanding, a continuous process would be designed and controlled
117 such that the mixture has the desired properties engineered when it is made. Many of the batch
118 upstream steps are not needed in continuous processing, particularly those at the interface of
119 upstream and downstream. For example crystallization and drying of the active might not be needed
120 at all. Additionally, filling of the bulk active and transportation might not be needed, nor removal and
121 dosing of the active, in downstream batch processing.
122

123 The continuous manufacturing plant could be capable of running constantly 24/7 for 50+
124 weeks/year, with no significant downtime for major cleaning (except in product or process
125 changeover), as is the case in other industries ranging from foods to petrochemicals. For
126 pharmaceuticals, such a process easily affords an annual production of 1 billion tablets, which
127 translates to only 120,000 tablets per hour, a throughput that is typical of a single pilot-scale line
128 using conventional technologies.
129

130 Because continuous processes are run under a constant state of control, dynamic aspects are
131 minimized, and dynamics such as transients associated with start-up and shutdown can be controlled
132 accurately so that products are within specifications all (or almost all) of the time. Along these lines,
133 continuous processes are controlled using detailed process models, which themselves are used in
134 advanced algorithms, leading to a much lower risk of going out of specification than batch processes.
135 Because of in-line process analytical technology (PAT) tied to the control system, the dream of real
136 time release (RTR) becomes a reality in a natural way, as part of the process approach. And in the
137 rare case of process perturbations, real-time rejection of small quantities of non-conforming product
138 can be performed without sacrificing the defined batch. The processes themselves are more robust,
139 leading to lower risk of stock-outs.
140

141 Furthermore, a manufacturing train for production of Phase III clinical materials could be developed
142 so that it is the commercial process, run for a short time for clinical supplies and year-round for
143 commercial production. Thus, a scale-up step is skipped, allowing reduction of critical path timeline
144 and reduced risk of development and manufacturing delays.

145 **2.1. Heterogeneous versus Homogeneous Processing**
146

147 We that expect that many, if not most, continuous processes that are developed in the near future
148 will be ‘heterogeneous processes.’ These are processes in which the components tend to segregate, a

149 problem that must be controlled throughout. These processes will be designed by leveraging existing
150 powder handling technology (i.e. incorporating common drug product formulation unit operations)
151 as many current drug product unit operations inherently have continuous flow or semi-continuous
152 flow (e.g. roller compaction, tablet compression). The focus of this initial approach will be in the
153 integration of these unit operations into a single line. Product quality is assured during processing by
154 using in-process monitoring by PAT and/or parametric control. Such an approach will benefit from
155 no open manual handling of actives, increased safety, smaller equipment footprint and shorter
156 processing times. However, these processes are far from achieving the full benefits of continuous
157 manufacturing and have the tendency to become 'Rube Goldberg' processes. Due to the familiarity of
158 the technologies involved, however, they are easier to develop from a technical standpoint and from
159 the standpoint of obtaining managerial and regulatory approval. For example, an existing batch
160 process, consisting of steps such as blending, granulation, milling, blending, tableting and coating
161 could be replaced with a corresponding continuous process incorporating the same steps. This flow
162 process would still have many of the advantages discussed above, but would likely be far from
163 reaping the full benefits of continuous processing. There would still be significant powder transport
164 challenges, unnecessary process steps that need to be eliminated, and higher risk of process issues.
165 Thus, we consider these heterogeneous processes as the initial step in the transition from batch to
166 homogenous continuous processing.

167
168 True continuous manufacturing involves 'homogeneous processes,' in which the components
169 processed exhibit no significant segregation on whatever the key length scale is, typically between
170 Ångstroms and microns. Thus, they need not be homogeneous on the molecular-level, as continuous
171 process steps can lead either to a solution, a melt, or a dispersion. The distinguishing feature is that
172 the active-exciipient combination is engineered to have the key properties needed in order to directly
173 make the final dosage form. For example, the synthesis and work-up can deliver the active in a
174 purified solution in which the excipients can be added and dissolved. Then the solution can be dried
175 and made into the final dosage form. Alternatively, the active and excipients can be melted or the
176 active can be nucleated on excipients. Another approach is that the active can be crystallized
177 separately and incorporated with the excipients in crystalline form, followed by direct formation of
178 the final dosage form. Examples of such homogeneous processes include extrusion, spray drying,
179 thin film formation, electrospraying and electrospinning, and injection molding and calendaring, as
180 discussed below. Homogeneous processing offers the true potential of continuous manufacturing.
181 Because homogeneous processing utilizes different technologies and it naturally involves integration,
182 it will necessitate different organizational approaches for both development and manufacturing.

183

184 **3. Challenges and Barriers**

185

186

187 Why, given the tremendous benefits of continuous manufacturing, has it not become the industry
188 standard? The main reason is a 'business as usual' approach embraced by a highly conservative
189 industry. Specifically, it has been seen that new manufacturing approaches must be proven both
190 technologically and financially superior, and tied to a product before widespread adoption will take
191 place. This leads to the 'chicken and egg' conundrum that technologies must be already adopted for
192 the industry to adopt them. This 'Catch-22,' coupled with the fact that process development and
193 manufacturing have not had a high profile in the pharmaceutical industry, has led to the adoption of
194 continuous processing being overly slow. Typically, pharmaceutical companies perform low-level
195 investments in new technologies to assess viability, and intensify those efforts only when tied to a
196 specific product. For equipment manufacturers, innovation in manufacturing equipment tends to be
197 incremental since these companies' main customers are in the pharmaceutical industry, which tends
198 to be more averse to adopting new manufacturing technologies.

199

200 Part of the 'business as usual' approach is rooted in the fact that the industry is highly regulated. US
201 regulators have been saying for years that the industry should adopt continuous manufacturing, and
202 a few companies have filed for select processes to be continuous. But companies, rightly or wrongly,
203 are wary of regulatory filings that consist of anything unconventional. These perceptions create a
204 vicious circle, in which lack of attention to, or investment in, manufacturing innovation leads to lack
205 of demonstrated value, which leads to lack of investment, etc. An additional concern is that the
206 pharmaceutical companies seek approval for their products worldwide; while FDA and select other
207 agencies may be forward-looking in this regard, continuous processing may not be approvable by
208 other global regulators.

209
210 The good news is that this is starting to change. Some regulatory agencies are pushing the industry
211 towards continuous manufacturing and are working to break down both real and perceived
212 regulatory obstacles. As the benefits of continuous manufacturing are understood more and more by
213 management, investments are being made that overcome the view of continuous manufacturing
214 being a complex and progressive approach to process development and manufacturing. This will lead
215 to continuous manufacturing becoming more and more prevalent. The question then becomes not
216 whether or not the industry should adopt continuous manufacturing, but how and when it will do so.

217 218 **3.1. Business and Organizational Challenges**

219
220 A perceived hurdle for industry in moving toward a continuous manufacturing paradigm is the
221 established batch asset-base: whereby significant capital was invested in batch manufacturing during
222 the rapid Pharma expansion during the 80's and 90's. However, capital investment in a new
223 continuous manufacturing plant could be offset by substantial savings, including savings in API
224 development costs, in addition to reducing or eliminating scale-up risk. Furthermore, continuous
225 manufacturing could substantially reduce the costs of API during development. Overall, such an
226 approach allows for rapid product development while naturally realizing the full vision of Quality-by-
227 Design (QbD), due to built-in process understanding.

228
229 In a commercial manufacturing plant, continuous manufacturing has the potential to realize a true
230 'lean manufacturing' paradigm and many benefits in the quality, operational, environmental, and
231 financial areas. These benefits arise through continuous process monitoring and control, lower
232 energy consumption, higher production yield, and shorter cycle times. Continuous manufacturing
233 also requires a smaller, more highly skilled workforce and smaller plant footprint making it ideal for
234 implementation in the United States, which would allow manufacturing to be in close proximity to
235 R&D centers. This can stimulate further innovation and ensure a more seamless transition from
236 development to commercial manufacturing. Given all of these benefits, it is envisioned that the likely
237 first step of most Pharma firms will be to convert, or integrate, many existing batch operations into a
238 continuous manufacturing plant (heterogeneous processing) prior to investing in a true
239 (homogenous) continuous manufacturing operation.

240
241 Secondary, or emerging, markets, bring a unique set of opportunities that can often be best
242 addressed by a continuous manufacturing strategy. For example, local manufacturing is often
243 required by governments in order to speed access to markets or gain access in the first place. When
244 this is the case, a small, flexible facility, which can meet the local or regional demand for a multitude
245 of products, is often desired. Continuous manufacturing, with its small facility footprint and high
246 turnover capability, can often meet these needs. Admittedly, the desired personnel capabilities may
247 not currently exist in secondary markets, but the robustness of steady state operation, coupled with
248 automated systems, training, and online, remotely accessible PAT can counteract the lack of local
249 talent with the desired skillset. Although it can be difficult to maintain facilities located within
250 secondary markets, portable manufacturing systems ('factory on a truck') could ease maintenance by
251 allowing entire facilities to be relocated to centralized locations as necessary. Furthermore, in the
252 desirable case where additional capacity is needed quickly, additional portable manufacturing
253 systems can be rapidly deployed to meet market needs. Given these significant opportunities, it is

254 also imperative to engage regulatory authorities in secondary markets to develop ways to reap the
255 benefits of continuous manufacturing as well as addressing the challenges presented by secondary
256 markets.

257

258 **3.2. Challenges Facing Manufacturing & Development**

259

260 The continuous manufacturing paradigm faces many manufacturing and development-based
261 challenges, from the mindset of the engineers and scientists who develop the formulation and
262 process, to the quality units within a company, to the government regulators overseeing the industry.
263 When a technology is immediately enabling, and allows for new medicines, that would otherwise fail
264 in development, to reach the market, few question whether extra work should be done to enable
265 success. This has been the case for the development of amorphous solid dispersions, which are a
266 recent example of a new technology rapidly finding adoption within the pharmaceutical industry.
267 Specifically, amorphous solid dispersions have enabled formulations to be more efficacious at a
268 lower dose by increasing the solubility of otherwise poorly soluble APIs. In contrast to that example,
269 for continuous manufacturing, the payoffs are not immediate and the benefits are spread out through
270 research, commercialization, and supply. Thus, extra time and effort must be spent in research and
271 development, all for a payoff that may or may not be achieved years later when a product hits the
272 manufacturing floor and the market.

273

274 From a regulatory perspective, continuous manufacturing may present extra up-front work for the
275 regulator. In order for quality to be assured, a regulator must learn the new manufacturing process
276 and the potential failure points. Often, quality practices that were developed for batch processes are
277 blindly applied to continuous processes. Furthermore, the larger number of measurements seen in
278 continuous processing is often a hindrance, as more data increases the likelihood of chance
279 observations of out of specification production. To combat this, engineers, scientists, and regulators
280 will have to upskill in statistics, so that the new data presented by continuous processes can be
281 properly analyzed and understood.

282

283 Further additional training includes giving all process developers a better understanding of control
284 and the model-based approaches available. In addition, all process developers would benefit by a
285 better understanding of powder handling. Additionally, training gaps need to be continuously
286 identified and addressed. Ultimately, a new continuous process must be shown to be superior to the
287 alternative batch process, in order to convince those who hold the purse strings to invest, a challenge
288 at which the continuous process is expected to succeed. While many of these obstacles can be
289 overcome through exposure and education, eventually it is the higher quality achieved through
290 steady state operation and online analytics that will drive the acceptance of continuous
291 manufacturing by both internal and government regulators.

292

293 Early in development, limited resources demand that project teams design a formulation and process
294 that is 'fit for purpose.' In other words, resource expenditure must be limited before a potential
295 product is shown to be worthy in the clinic. After proof of concept is achieved for a particular
296 molecule, development typically moves towards a focus on the target product profile (TPP), which
297 addresses the requirements of patients and caregivers for a given product. Having achieved the TPP,
298 late stage development groups begin to focus on the manufacturing requirements such as long term
299 operational robustness, production scale and product cost. At this stage, a product will generally
300 have spent significant time in the clinic, and any formulation or process changes will be perceived as
301 a risk to both the timeline and product performance. Thus, programs that start at small scale with
302 batch operations often result in products at large scale being produced using batch operations.

303

304 Product development using continuous manufacturing requires a new mindset towards research and
305 development, and a certain amount of bravery. In order for the most benefit to be realized,
306 continuous processes must be embraced at the earliest possible stage. For any researcher, the
307 benefit of a continuous process towards conducting a sequence of experiments is rapidly realized.
308 With some simple automation, and perhaps scaled-down apparatuses, screening of both formulation

309 and process parameters can be rapidly achieved. This rapid execution, however, comes at the cost of
310 high material consumption rates. Ideally, equipment dimensions would be scaled down such that the
311 benefit of continuous processing can be achieved alongside low consumption rates, but
312 pharmaceutical equipment manufacturers are only now beginning to observe this opportunity. If
313 continuous processing is to be achievable early in the development cycle, testing of more
314 formulations and process conditions per kg of API would be expected to result in better formulations
315 and more robust processes. Because continuous processes are inherently more 'data rich,' new
316 information technology systems must be developed to collect, process, and analyze the rich data
317 streams that are generated with every experiment. These data streams should ultimately result in
318 higher quality products, as online analysis systems 'sample' a higher fraction of every batch,
319 sometimes by a factor of 100x or greater. Product filings will also become easier in some regards, as
320 more of the process space is sampled and more is known about each condition tested. Electronic
321 batch records become easier to implement as well, as does prospective process analysis and
322 continuous process verification, as each relies on an automated stream of high quality data for
323 optimal implementation. And once products developed with a continuous manufacturing mindset
324 reach commercial production, the compounding of benefits will begin to be realized. Hence, it is
325 envisioned that product development teams that fight the obstacles and adopt continuous
326 manufacturing strategies early in development will reap benefits not only for themselves, but for the
327 patients who need the product and the commercial production sites that supply it.
328

329 To achieve widespread adoption of continuous manufacturing technologies, new generations of
330 equipment, sensors and automation will need to be developed, together with approaches to perform
331 in-line tests such as friability, disintegration, and dissolution. This will most easily be achieved
332 through collaboration between equipment manufacturers, academics, and pharmaceutical
333 companies. In addition to smaller scale equipment, equipment manufacturers will need to work
334 together to standardize the connections between unit operations. New sensors will also need to be
335 developed, to address needs ranging from online particle size measurement to mass flow rates in
336 particulate systems. In a continuous manufacturing environment, system integration becomes of
337 high importance, as unit operations have to communicate in order to maintain control. Companies
338 that can serve as a 'one stop shop' will gain prominence, as the need for one manufacturer who can
339 provide equipment, sensors and control systems becomes a key desire. Finally, the challenge and
340 potential of 'big data' will become central, and systems that integrate sensing, automation, analysis
341 and control will become highly sought after.
342

343 **3.3. Overview of Technical Challenges**

344

345 There are several inherent technical challenges to continuous manufacturing that may be more or
346 less relevant depending on the specifics of the product. One is powder characterization and handling,
347 particularly for low-dose production, including process modeling. Another is how to do start-up and
348 shutdown as rapidly as possible with minimal waste. In general, it is a challenge to develop accurate
349 process operations models of various steps in a continuous process. Other challenges include
350 materials issues, such as build-up over long run times, loss in weight feeding, especially for cohesive
351 materials, maintaining mass balance with the lack of mass flow powder meters, material tracking
352 through system via residence time distribution (RTD), balance of need for system capacitance and
353 short residence time, and need for online PAT. Ways to address these are included throughout this
354 white paper and involve a combination of equipment technologies and control systems. Details of
355 technical challenges for specific technologies are discussed below.
356

357 Together with the fact that continuous manufacturing is the ultimate in lean manufacturing,
358 flexibility is a key aspect, whether in meeting a need to produce in the same line product with
359 different content of API or different products or different volumes during the year. This is an
360 important evaluation element for the design of a continuous line, in terms of size (capacity) and
361 modularity (different products) with the possibility to adopt different paths for the product through
362 various modules according to the formulation chosen. Consequently, if it is necessary to change
363 production on a line, the cleanability and the setup time become extremely important. Cleanup, in

364 this case, includes waste at the beginning, and end, of production. The need for flexibility is likely to
365 influence the level of continuity of the system, in terms of integration between upstream and
366 downstream.
367
368 Even homogeneous processing necessitates powders handling for precursor materials in chemical
369 reactions and blending excipients or even active materials. As discussed above, an annual production
370 of a billion tablets means 120,000 per hour of continuous production. If each tablet is 400 mg,
371 addition of a solid material at 1% of total weight means addition at about 480 g/hr. This is certainly
372 feasible, but at a factor of 10 lower production, achieving accurate doses of powders and assuring
373 smooth flow can be a challenge.
374
375 A related challenge is the development of small-scale equipment for early studies. Small-scale
376 synthesis may be routine but small-scale spray drying or melt extrusion is potentially more difficult,
377 especially blending and coating. Spray drying, in particular, and related methods, which use pure
378 streams of actives or active/excipient solutions, could have many advantages in that the effects of the
379 solid state chemistry of the drug could be minimized, and amorphous dispersions or pure crystals
380 could be made directly, depending on the desired formulation and the properties of the API molecule.
381 Solvent recovery could pose a challenge with spray drying, but in general it can be incorporated
382 seamlessly into a continuous process. A key question is how much should we invest in small-scale
383 equipment and know-how in general. Process development could benefit tremendously from this,
384 but there is a cost involved.
385
386 Clearly, the availability of small-scale continuous manufacturing lines capable of making clinical
387 supplies (even Phase I), which could then be scaled up for larger scale manufacturing, would be a
388 major advantage. This capability would significantly accelerate drug development, especially if the
389 small-scale equipment was predictive of larger scale processes. For example, a mini melt extruder,
390 only slightly larger than a ballpoint pen, is available as are mini spray dryers. Little is known about
391 the ability of these units to scale to larger manufacturing processes and they are too small to meet
392 demand even if run continuously. Additionally, little is known about the ability to incorporate these
393 units into a mini-continuous line.
394
395 One concern during continuous manufacturing is the modeling of variances, and how they might
396 propagate through a continuous process. Specifically, if a disturbance enters the first unit operation
397 in a series, the question arises as to whether that disturbance will spread out, and if so, by how much.
398 To answer this question, an in depth understanding of the RTD of each unit operation is required, as
399 this serves as the transfer function which translates how input variability is related to variability in
400 the output of each step. In addition to understanding each unit operation's transfer function, care
401 must be taken to understand the system capacitance and delay times associated with material
402 transport operations between steps. Because complex interconnected systems with time delays are
403 inherently non-linear, care must be taken during design and testing of the individual and overall
404 system controls to ensure that the system dynamics do not become unstable and lead to control
405 system runaway or other chaotic phenomena. The careful design of mixing steps and buffer tanks in
406 a continuous process can be used to help smooth process dynamics, by dampening and delaying
407 process variability. Ultimately, it is expected that model-based control using knowledge of the RTD
408 would be a key element in aiding this process, and flow sheet modeling will enable testing of system
409 dynamics outside of the plant environment.
410
411 Start-up and shut down are a key challenge particularly for the vision in which the pilot process will
412 become the commercial process, and scale-up occurs in time as opposed to volume. For an
413 anticipated billion tablet a year product, one might need somewhere between 10,000 – 5,000,000
414 tablets for Phase III, meaning, in many cases, fewer than a single day's output. To make these cost
415 effective, start-up and shutdown would need to be minimal. This can be achieved by minimizing
416 system volume to the extent possible, as the average system residence time for a given throughput
417 will increase proportional to the holdup volume, and typically 3-5 residence times must pass before a
418 first-order process achieves steady state. RTDs of all of the various units must be taken into account,

419 as getting products to specification will take as long as the slowest element of the process. Smart
420 sequencing of unit operations during start-up and shutdown can further decrease losses. For
421 example, a continuous blender could be filled completely, and mixed in a batch mode (with no
422 discharge) for a few moments prior to allowing material to pass to the next process step. Although
423 the material processed would not be considered steady state, it could still be processed so as to meet
424 the product's blend uniformity specifications, and thus would be considered good material.

425

426 **3.4. Key Choices and Design Constraints**

427

428 In determining a plan of action for moving to continuous processing, companies will need to make
429 design choices that may lead to constraints. These include:

430

- 431 • Multiple small-scale operations versus fewer (or one) large-scale operations
- 432 • Custom lines for each drug versus platform lines
- 433 • Use of existing technologies versus incorporation of new technologies
- 434 • Determination of how much front end loading of research to invest in, particularly given
435 attrition rates
- 436 • How integrated the approach should be for commercial production and during product
437 development including scale-up

438

439 What companies will decide will depend on a number of factors including a product's timeline,
440 process lifetime, specific nature of their business in various countries, size and nature of their
441 pipeline, and their willingness to take on higher risk for higher rewards. Eventually, maximum
442 benefits will be achieved by realizing the full vision of continuous, but during the transitional period,
443 companies will need to pursue strategies that make sense for them, while continuing to pursue the
444 ultimate vision.

445

446 **4. Technologies for Continuous Final Dosage Formation**

447

448 **4.1. Overview**

449

450 The true benefits of continuous manufacturing can be harvested when new technologies are
451 implemented. This means designing a continuous process with the mindset of continuous
452 processing. This mindset is difficult to acquire given the inertia of batch processing between both
453 process designers and managers. Thus, in many companies there is likely to be a transitional period
454 during which batch approaches are converted to continuous. This will result in lower perceived risk
455 and lower up-front investment (although it does not result in maximal benefits). The key to doing
456 this, however, is to avoid the 'Rube Goldberg problem,' in which process elements are added to
457 correct problems of other process elements, the opposite of what continuous manufacturing is
458 supposed to be.

459

460

461 **4.2. Upstream-Downstream Interface**

462

463 As discussed above, maximum benefits of continuous processing can be achieved by process
464 integration, when the upstream and downstream parts of the process are combined seamlessly.
465 When this occurs, there are two major routes by which the active can be transferred from the
466 upstream to the downstream part of the process. One of those is as a solid, either dried or in a slurry,
467 and the other is dissolved in a solution.

468

469 If the active is transferred as a solid, the process as a whole should be designed so that the particle
470 size is at the final specification and the residual solvent can either be incorporated into the final

471 dosage form process (e.g. as an granulation agent) or can be removed by drying. In general, the
472 process should be designed as a whole, so that what occurs downstream does not involve corrections
473 of what should have been done upstream.

474

475 **4.3. Powder Handling**

476

477 **4.3.1. Transitional Technologies and the Challenges of Powder Handling**

478 Today, tablets represent the majority of pharmaceutical solid dosage forms available on the market.
479 Of this group the vast majority are produced through batch processing of one of three general
480 pathways: wet granulation, dry granulation, or direct compaction.

481

482 Wet granulation (the original solids manufacturing approach) involves first spraying a liquid onto a
483 bed of powder while it is mixed by pneumatic or mechanical means and then removing the liquid
484 from the material with a second process step. The water sprayed into the bed serves as a means to
485 bind individual particles together into a larger agglomerated particle. The purpose of creating the
486 agglomerated materials is to create a powder, which will flow better and not be prone to the
487 segregation problems often found in blends composed of the smaller sized primary particles. It is a
488 common practice to mill the material after drying to break down any larger sized agglomerates.

489

490 The most popular alternative to wet granulation is dry granulation, in which pre-blended material is
491 continuously compressed between two cylinders (referred to as rollers) in a device known as a roller
492 compactor to produce a compacted strip of material known as a ribbon. After the ribbon has been
493 formed it is converted back into a granulation by milling the ribbon into smaller agglomerates. As
494 with wet granulation, the goal is to produce a granulation that has superior flow properties and a
495 lesser propensity to segregate based on constituent size. The main strength of the dry granulation
496 approach is it does not require a complex/costly drying step.

497

498 The final, least used, and newest approach to tablet manufacturing is direct compaction. In direct
499 compaction, material is blended and fed directly to a tablet press for compression. The advantage of
500 the direct compaction approach is its simplicity. Its main drawback in batch operation is that the
501 powder needs to have good flow properties and not be prone to segregation.

502

503 In the pharmaceutical industry, all of the three pathways, for the production of tablets, described
504 above have been used in discrete batch-wise based operations., There is, however, no fundamental
505 reason that these process steps have not, or could not, be done continuously. In fact, all of the batch-
506 wise unit operations used in the pharmaceutical industry have continuous analog(s) in other fields of
507 manufacturing such as foods, petro-chemical and agriculture. In the past 10 years, the industry has
508 begun to investigate the potential of continuous manufacturing for solids dosage form. To date, five
509 companies offer some form of continuous manufacturing platforms for solid dosage production (GEA,
510 Glatt, Lodige, LBBohle, Gericke/Gerteis).

511

512 The three tablet production routes described above use a combination of six basic unit operations:
513 weighing/dispensing, blending, granulation, size reduction, compression, and coating. Continuous
514 equipment capable of fulfilling each of these roles is described below.

515

516 **4.3.1.1. Weighing/Dispensing – Continuous Feeding**

517 The objective of the weighing/dispensing operation is to measure out the correct ratio of ingredients
518 specified to compose the final product. In a continuous operation, this requires feeding each material
519 at a specified *rate* such that the final product will have the proper composition. This is accomplished
520 through the use of Loss-in-weight (LIW) feeders. LIW feeders are comprised of a hopper mounted on
521 top of a positive displacement screw feeding system all of which is constantly monitored by
522 scale/load cell. When the screws are in motion, powder is fed from the material hopper into the

523 process and the total weight of the screw feeding system and the hopper decreases at a rate
524 equivalent to the rate at which material is being fed into the system. The scale, on which the feeder is
525 mounted, continuously monitors this loss in weight and can adjust the screw speed so that the rate at
526 which material enters the system remains on target.

527
528 However, the granular nature of the material being fed leads to a limit on how accurately this LIW
529 loop can control the addition of the material. This is due to the fact that powder streams do not act
530 like either a solid or a fluid. When energy is applied, they can be made to flow and in special
531 circumstances act very much like a liquid (e.g.. fluid bed). When energy is removed, they can hold
532 shape and act like a solid (e.g. angle of repose measurement). This complex behavior leads to
533 variations in the interaction between a feeding screw and the material both within the screw and at
534 the exit of the feeder. This leads to variations in the feeding rate even under strict loss in weight
535 control. At high feeding capacities the discrete nature of the powder stream becomes less significant
536 and feeding accuracy is greatly improved. The main challenge is in feeding materials accurately at
537 slow speeds where the variations can become large compared to the rate at which the material is
538 being fed. Therefore, minor components (lubricants and disintegrants) are often the most susceptible
539 to feeding limitations.

540

541 **4.3.1.2. Blending**

542 The most common type of continuous blender is known as a tubular blender. Tubular blenders are
543 comprised of a horizontal (or nearly horizontal) tube with a bladed impeller running down its central
544 axis. Material is typically fed into one end at a steady state and the blades of the shaft move it along
545 the length of the shaft. At the far end of the tube there is an exit where the material is passed to the
546 next process by gravity.

547
548 The mixing objective in continuous blending can be categorized into two separate modes: radial and
549 axial. Radial mixing can be explained by considering two powders, A and B, being fed into a blender
550 each on opposite sides of the blender's axial center line at a constant speed. A snapshot of a radial
551 cross section of the blender tube near the entrance at steady state would show two unblended
552 powders (See Figure 1). If the blender is properly designed and operated, a snapshot of the radial
553 cross section near the exit of the blender would show two powders blended together. The key aspect
554 of radial mixing is that it is a steady state process, and can largely be considered time-invariant.

555
556 ,Radial mixing alone, however, does not present a complete picture. As described above, some
557 variation in the rate at which granulator materials are fed will exist for all feeders and can be
558 significant for minor components, which require lesser-feed rates. If a continuous feeder simply
559 radially blended the incoming materials, then any noise from feeding would pass right through the
560 blender and end up as variation in the final solid dosage form. As a consequence, a continuous
561 blender should be designed to encourage incoming powder, which comprises the process stream, to
562 spend a variable amount of time within the blender. The larger the variation in the amount of time
563 the constituent particles of the blend stay in the mixer the more the mixer is averaging out the noise
564 of the upstream process. This is referred to as axial mixing and it can be visualized as mixing along
565 the length of the cylinder. How much axial mixing is desired will depend on the specifics of the
566 process, but should be engineered in. Axial mixing tends to average out properties which could make
567 it easier to keep products within specifications and get them within specifications earlier during
568 start-up and shut-down, but it also leads to an inherently larger residence time, which can make it
569 longer for products to get into specifications.

570

571 In a continuous process, it is critical to understand that the feeding and blending systems must be
572 designed to work in concert. The accuracy with which the available equipment can dispense each
573 component must be fully understood, as this leads directly to the degree of axial mixing that is
574 required in the blending step. A suitable blending system must be designed to ensure that the level of
575 variation present for each component in the process will be averaged back to within the product

576 specifications for concentration, but it must not provide so much backmixing as to lead to an
577 unnecessarily long residence time. Process modeling is expected to play a major role in determining
578 the balance between axial and radial mixing that results in the design of a high performance process
579 given the specific material feeding characteristics for a given product.
580

581 **4.3.1.3. Granulation**

582 *Wet Granulation*

583 The present standard approach to wet granulation is the fluid bed granulator. In a fluid bed
584 granulator, the powder material is fluidized by air and granulated by spraying the bed with a binder
585 solution. After the spraying phase is completed, the bed can be kept fluidized until the air movement
586 dries the bed to the specified level.

587
588 While not common in the pharmaceutical industry, fluidized beds are often run continuously. They
589 come in two categories, troughs and rounded beds. In the trough approach, a linear bed is fluidized.
590 At one end, the additional material is fed, which raises the level of the bed and pushes the fluidized
591 bed towards the far end where the material exits to the next process. Spray nozzles can be placed
592 along the length of the bed to spray binder and agglomerate the particles. The last length of the bed
593 can then be used to dry the particles. The rounded bed approach involves continuously feeding
594 material into a conventionally shaped fluidized bed while the bed is being sprayed. When the bed is
595 at its desired volume, material is removed at the same rate that it is fed in and the stream of
596 agglomerates is classified by size. Material found to be too small (under-agglomerated) is re-
597 circulated back into the bed for further processing and the larger material is allowed to progress to
598 the next unit operation. In this configuration a second fluidized bed would be needed for drying.
599

600 *Dry Granulation*

601 Roller compactors are fully continuous processes. They continuously feed powder to the rollers,
602 which produce the ribbon. The ribbon is continuously fed to the mill, which then transforms the
603 ribbon back into a granulated material. No changes are needed and the roller compactors can be
604 integrated into a continuous line as they are.

605

606 **4.3.1.4. Size Reduction**

607 The most commonly used size reduction equipment in the industry is the Conical-mill, commonly
608 referred to as the co-mill. Co-mills push incoming material through a conical screen using an
609 impeller, which forces material near the screens surface through the spaces in the screen. Co-mills
610 are inherently continuous equipment and can be used without alteration. However, the manner in
611 which they are operated will be somewhat different. Currently, the material to be milled is dumped
612 on top of the co-mill the mill speed is set and the mill is run until all of the material has run through
613 the mill. In a continuous process, the material will be constantly feeding the mill and it will be
614 necessary to match the speed at which the mill is processing material to the speed at which the line is
615 running.

616

617 **4.3.1.5. Compression**

618

619 Tablet presses are another example of equipment that currently runs continuously. The main
620 challenge with adapting a tablet press to a continuous line is devising a control strategy to match the
621 production rate of tablet press to the rate at which it is being fed materials. One strategy involves
622 modulating the press turret speed to change the overall mass flow rate, and using this mass flow rate
623 control to keep the powder level constant at the inlet of the press. In batch compression tablet press
624 speed is typically not varied and therefore special attention will need to be dedicated to
625 implementing an effective level control system in continuous. When successfully implemented, the
626 risks for powder flow issues and segregation can be significantly reduced for continuous direct
627 compression.

628
629

4.3.1.6. Material Handling Challenges in Homogeneous Processing

630 Even after a paradigm shift towards homogeneous processing, it is highly likely that granular
631 materials will need to be fed into the process. The engineering framework for dealing with these
632 additions will be the same as described above in the feeding/blending system. The feeding system
633 will need to be characterized for how accurately it can dispense the material, and then the system
634 will need to include enough back mixing to adequately time the average of the process stream to
635 keep the product within its pre-determined specifications.

636
637

4.4. Emergent Continuous Processes for Homogeneous Production of Final Dosage Forms

639

640 The key final dosage formation technologies include homogeneous technologies, primarily with
641 polymer excipients. If actives and excipients are blended in solution, crystallization must be
642 addressed, either obtaining the desired crystal form or avoiding crystallization for a desired
643 amorphous dispersion or solution. Alternatively, mixtures can be formed with crystalline active
644 particles and even particles of excipients in a solution with other dissolved materials. Either way, the
645 properties of the blend must be tuned so that the final dosage form can be made directly. A key issue
646 is the dosing of the active, whether small or large. Small dosing may be stabilized as a solid
647 amorphous solution, thereby also allowing dispensing via a solution, instead of a powder. In this
648 case, the properties of the mixture or blend are controlled primarily by the excipients and can be
649 tuned in a relatively straightforward manner. For large dosage pharmaceuticals, the properties of
650 the active will have a large effect on the properties of the final blend, making it much more difficult to
651 tune. We describe the following:

652

- 653 • Spray drying
- 654 • Electroprocessing
- 655 • Casting
- 656 • Injection molding
- 657 • Hot melt extrusion
- 658 • Printing
- 659 • Continuous coating
- 660 • Ultrasound Compaction

661

662 Spray drying should be familiar to most in the industry. It is an inherently continuous technology in
663 which a solution is sprayed through a nozzle into a vessel in which a gas such as nitrogen is blown in
664 order to dry the airborne droplets. Typical droplet sizes are on the order of 10-200 μm . In order for
665 these droplets to dry sufficiently, commercial spray drying equipment is often required to be quite
666 large (several stories high) although for process development there are small-scale spray drying
667 apparatuses that can fit in a typical laboratory.

668

669 Spray drying is particularly advantageous for amorphous products, which dissolve fairly easily, since
670 on the one hand the particle sizes can be on the large side for pharmaceutical products, and on the
671 other hand, drying might be fast enough such that adequate crystallization might not occur.
672 Annealing can be used to affect crystallization, but that might not be sufficient for active material in a
673 polymer matrix.

674

675 Having extolled the virtues of spray drying, it is important to note that as currently practiced, the
676 preceding and subsequent steps are not inherently continuous, and these would need to be modified
677 to integrate seamlessly into a continuous process. In addition, the range of its applicability needs to
678 be determined. Specifically, to become truly continuous, the challenge of continuous mixing during
679 polymer/drug/solvent solution preparation must be resolved. Although continuous inline
680 solid/liquid mixers are available, the slow dissolution dynamics of polymers can limit performance.

681 Furthermore, after the spraying process is complete and the semi-dry polymer/drug particles exit
682 the primary drying chamber, they are often collected in a bulk vessel, and held in a wet state until a
683 subsequent secondary drying step. In most circumstances, this secondary drying step is needed to
684 reach ICH solvent limits, and is currently practiced as a batch process with long cycle times. Truly
685 continuous spray drying would need to conduct this secondary drying in a more time efficient
686 manner using some of the continuous drying technologies described elsewhere in this paper, starting
687 from the moment of powder collection out of the primary drying chamber.
688

689 Electroprocessing is a related approach to spray drying, but there are some key differences. First, in
690 addition to droplets, fibers can be produced. Processes that produce the former are called
691 electro spraying and the latter electrospinning. Because of the electrohydrodynamics of
692 electroprocessing much smaller shapes can be formed, droplets and fibers with submicron
693 diameters. Furthermore, in electroprocessing, droplets and fibers can be formed through nozzles
694 (generally at low rates) or from a liquid surface with an electrode underneath. The latter is generally
695 done on a spinning cylinder electrode and is called free-surface electroprocessing. Electroprocessing
696 can be performed with single-phase fluids or with heterogeneous mixtures, for example solid crystals
697 suspended in a polymer solution. Once electroprocessed material is generated, it will need to be
698 shaped into a final dosage form by a compression and cutting operation or a combination of the two.
699

700 Another way to make a final dosage form is liquid casting. The challenge in doing this is to get
701 acceptable drying, particularly if a tablet is cast directly. Another approach is to cast thin films, dry
702 them sufficiently, and then shape them into tablets or whatever the final dosage form is. Casting can
703 be performed with the active in solution or entrained as a powder. Another exciting approach for
704 casting is that the excipients can be cast and dried, followed by nucleation of the active directly on
705 the excipient film surface. These surfaces can be designed either with patterns or with surface
706 functional groups to yield the desired polymorph, crystal size distribution, and morphology.
707

708 Tablets are relatively simple shapes that can be directly formed when an API is mixed with a flowable
709 excipient such as in polymer dispersions. Injection molding is one technique that can be used, as it is
710 a technology that has been used for decades to make inexpensive plastic parts. These parts can be
711 simple in shape or extremely complex with tight specifications of features. More recently, the tablet
712 geometry has been directly formed through a process called calendering, with equipment available
713 through manufacturers such as Dr. Collin GmbH. Whatever the shaping equipment, it is usually
714 paired with the extrusion process and will use typical melt extrusion methodologies as described
715 elsewhere in this manuscript,
716

717
718 Another technology is printing, in which either separate droplets of active and excipient or solutions
719 of actives and excipients are formed into a tablet via an approach such as ink-jet printing. This
720 approach promises tight control over dosing and excipient amounts, but can have significant issues
721 with drying.
722

723 Application of ultrasound leads to a transition of polymers into (semi-) liquid state, offering the
724 possibility of embedding drug into polymer matrices. Hence, UltraSoundAssistedCompaction (USAC)
725 might be an alternative to common techniques in solid dispersion preparation. Critical parameters
726 are identified as follows: ultrasound energy, compaction force, amount of powder and the distance
727 between sonotrode and product slug.
728

729 In all of these technologies, forming discrete final dosage units will be necessarily semi-continuous,
730 for the very reason that those dosage units are discrete. Developing robust ways to keep these final
731 dosage formation processes running for long periods of time without disruption will also necessitate
732 new technological approaches.
733

734 Of course, this is just the beginning and innovative research will no doubt develop a range of new
735 technologies as continuous processing continues to spread.

736
737
738
739
740
741
742
743
744
745
746
747
748
749
750
751
752
753
754
755
756
757
758
759
760
761
762
763
764
765
766
767
768
769
770
771
772
773
774
775
776
777
778
779
780
781
782
783
784
785
786
787
788
789

4.5. Excipients and Formulation

A general challenge with the above approaches is how to choose excipients to create a formulation, which has the right pharmaceutical properties (*in vivo* release and PK), stability, and processing properties (particularly mechanical properties that will allow shaping into the final dosage form). A key challenge is proper *in vivo* release. In contrast to traditional powder tablets, in which disintegrants can be added and solvent can easily get to them through pores in the tablet, leading to tablet swelling and disintegration, the above dosage forms do not have typically have pores between solid particles.

One solution is to engineer pores into the dosage forms either with bubbles or by drying individual droplets sufficiently before making the final dosage form, such that solvent can access the core of the tablet. Another solution is to choose a formulation that dissolves rapidly *in vivo*, either directly, or by putting in a network of rapidly dissolving material.

Another key set of properties, in addition to stability, is that the blend has the proper processing properties. Whatever the technology, it needs to be able to flow, be deformed, shaped, and/or compressed with differing target properties depending on the final dosage formation technology used. Current batch formulation approaches that have been worked out for powders are most likely not appropriate for continuous processing. This opens a whole new realm of formulation approaches and possibly a need for new excipients.

Possibilities for future new excipients are best understood by studying the example of melt formulations, and similar examples can be studied for other process technologies such as spray drying. Melt formulations, using specialty polymer excipients, are anticipated to play a central role in the future continuous manufacturing of homogeneous dosage forms due to the simplicity and wide applicability of the process. Current polymeric excipients used for homogeneous solid dosage manufacture often exhibit limitations such as:

- High processing temperatures
- Narrow processing ranges
- Low dissolution rate of drug into excipient matrix
- Limited physical stability
- High hygroscopicity
- Sub-optimal drug dissolution rate and low solubility (or supersaturation) *in vivo*

To reduce processing temperatures and expand processing ranges, polymers with lower Tg can be used, but this often comes at the cost of reduced physical stability. To regain this physical stability, one option is to design polymers, which are thermodynamically stable when combined with drugs. This stability can be gained through specific interactions between the drug and polymer, whether ionic or hydrogen bonds, or simple hydrophobic interactions. Of course, the designers of drugs also have a role to play in achieving this future state, as higher potency drugs with a lower required dose will inherently be more stable in matrix formulations. Trends are already beginning to emerge towards more specialty excipients, whether copolymers with different monomer ratios, or substituted polymers with different side groups at varying levels and in varying patterns. An example of this can be seen by examining the substituted cellulosic polymers, and the variety and amount of functional groups that are bonded to the cellulose backbone to form new polymer grades. Looking towards the future, it is expected that many more options will become available, utilizing copolymers that are random and block, straight chained and branched, substituted and patterned, and the optimum will be selected via high throughput screening or computer modeling with the drug being formulated. Finally, upon development of an array of purposefully designed excipients, continuous manufacturing of homogeneous dosage forms can begin to take shape.

790 **4.6. Transitional Continuous Technologies**

791
792 Transitional approaches, in which batch technology are converted to continuous, include granulation,
793 blending, and direct compaction. Roller compaction and extrusion are ways of carrying out
794 granulation, and extrusion can be used directly for blending. There currently exists equipment to
795 perform all of these in stand-alone continuous operations, but integration still remains an open
796 challenge.

797 798 **4.6.1. Continuous Drying**

799
800 Continuous drying technology development will be a key aspect of continuous process development.
801 The challenge will be to achieve sufficient drying in a reasonable amount of time. We envision
802 multiple types of drying approaches utilized even in a given process, depending on specifications and
803 the degree to which the material holds the solvent. Approaches include, squeeze drying, belt drying,
804 drying through a screw, and fluid bed drying. Other approaches include washing with solvents that
805 extract the hard to dry solvent, and overall process design to streamline drying.

806 807 **4.6.2. Continuous Coating**

808
809 Typically, film coating is done in a process by which tablets are sprayed with a pigment containing
810 polymer solution while being tumbled in a dry air stream. The drying air removes moisture, leaving
811 behind an elegant tablet coated by a thin film of colored polymer. Although most film coatings are
812 added for taste masking or elegance purposes, film coating is also sometimes used to add functional
813 coats to tablets, which can delay or control release of the API until the desired time after
814 administration. While film coating of batches from 1kg to 300kg is common, production cycles can
815 run for more than 2 hours between pan loading, spraying, and unloading.

816
817 Two options are often discussed in the context of continuous manufacturing. Continuous film coating
818 is the name given to the process where tablet cores are loaded at one end of a long rotating
819 perforated cylinder, the tablets pass through a multi-gun spray zone, and coated tablets are
820 simultaneously removed from the opposite end. While this design is truly continuous, it suffers from
821 high dispersion at low mass flow rates, leading to high variance in the amount of coating applied. As
822 an alternative, short cycle duplex batch coaters operate by having one coater loading or unloading
823 while the second coater is spraying. By operating the two coating cycles out of phase, a semi-
824 continuous flow is maintained. Although dispersion is not a problem in this arrangement, the short
825 cycle duplex batch coaters do not enable the same turndown ratio afforded by the continuous coating
826 process, and thus are more difficult to operate when production conditions vary. Both approaches
827 warrant consideration when designing a process train that necessitates a film coating operation.

828 829 **4.7. Technical Approach to Development of Continuous Equipment**

830
831 As described above, there is a “Catch-22” to the development of continuous equipment, as
832 pharmaceutical manufacturers want equipment that has been tried and tested, and equipment
833 manufacturers will not make significant investments in new equipment designs unless they are
834 assured customers. Thus, the major way out of this conundrum is for pharmaceutical manufacturers
835 to accept the risk, and start investing in new approaches while trusting that the newly developed
836 approaches will provide the financial benefits to justify the initial investment. While pharmaceutical
837 manufacturers must lead the way, equipment manufacturers should also be proactive in making
838 investments in transitional continuous approaches and also at least research investments in
839 equipment for true continuous operation. The equipment manufacturers who do not do this might
840 very well find themselves left out of future markets, as equipment manufacturers who have not
841 previously had a presence in the pharmaceutical industry, but do have equipment suitable for
842 continuous, will start to target this new and substantial market.

843

844 **4.8. Systems Engineering, Characterization, and Control for Final Dosage Form**

845
846 The Control white paper, and others, covers the overall approach to process design and control. Here
847 we mention the specific challenges in those areas to continuous final dosage formation. The
848 challenges are two-fold: accurate and robust models are difficult to obtain and inline analytical
849 approaches are difficult. On-line analytical approaches to characterize solid materials are especially
850 challenging, including particle size determination, composition, and crystal form analysis.
851 Nevertheless, approaches exist to perform characterization, even of solids, and we envision that, on
852 the one hand, as more and more investments in continuous are made, better and better models will
853 be developed, and better inline analytical methods will be developed on the other. In fact, the two go
854 side by side, as better analytics will lead to better models and vice-versa. All of these, together with
855 model-based control, will make continuous manufacturing processes streamlined, of high quality,
856 lower waste, and increase value.

857 858 **5. What the Industry Should do and Timing Including Resource Allocation**

859 860 **5.1. What Each Company Should Do**

861
862 Given the projected advantages of continuous manufacturing, the industry should initiate continuous
863 manufacturing efforts immediately. Each company should go through its product (development and
864 in-line) portfolio and choose one or more products for some degree of continuous manufacturing.
865 This could be a life-cycle management product, but the real value is in a new product, chosen as early
866 in the development phase as possible, for example at proof of concept in the clinic. Of course, a new
867 product in development has a much higher risk of attrition, so ideally multiple products would be
868 chosen. In addition, a company would have to be highly confident that the choice of continuous
869 manufacturing would not delay regulatory approvals across global markets. To the extent possible, a
870 platform approach should be chosen for phase III and commercial production, thus, reducing
871 expenses and the risk that all chosen products would not go at least to Phase III clinical trials.

872
873 As the initial investment required to develop a continuous process is likely to be more than that of a
874 corresponding batch process, and because new equipment would likely need to be purchased (and
875 even resources spent on development of the equipment), management should consider this to be a
876 research investment for which the payoff is likely to be not so much with the given continuous
877 process, but with the ultimate benefits to continuous implemented in the company as a whole. The
878 future of pharmaceutical manufacturing is continuous. The earlier a given company gets there, the
879 sooner it will reap the benefits.

880 881 **5.2. What the Industry as a Whole Should do, including companies, regulatory bodies, and** 882 **universities**

883
884 The most prevalent comment during the International Symposium on Continuous Manufacturing
885 (May 20-21, 2014) was to include analyses of examples of continuous manufacturing, in addition to
886 case studies. These would also need to demonstrate the benefits of homogeneous over
887 heterogeneous processing, particularly given the fact that many current heterogeneous assets are
888 already fully depreciated and assets for homogeneous processing would require new investments.
889 This would be a perfect opportunity for a university-government-industry partnership. This analysis
890 should include benefits and detriments of new technologies and homogeneous vs. heterogeneous
891 processing, in addition to evaluation of non-tablet dosage forms. Several delegates specifically
892 suggested an analysis on liquid-dosage forms, for which continuous manufacturing should provide a
893 huge benefit and be easier to implement than solid dosage forms.

894
895 In addition, there was considerable interest in understanding the need for and potential of small-
896 scale equipment technologies. This includes current limitations and ways to break forward from

897 those limitations, but more so needs, particularly for small scale powder handling during process
898 development and production of relatively small volumes.

899

900 Furthermore, the industry should consider what approaches would be 'pre-competitive' such that the
901 industry as a whole would benefit versus what would need to be patented or kept as proprietary. In
902 addition, educational needs should be enumerated and ways to address them developed. This could
903 certainly be done in part in companies themselves, but would also likely benefit tremendously from
904 university engagement.

905

906 Clearly, then, a potential university-industry-government partnership could be in the area of
907 education and training. All three entities could collaborate to develop curricula that would address
908 the knowledge and skill gaps across the industry.

909

910 Acknowledgements

911

912 We would like to thank our Frank Roche and Sonja Sharp for valuable comments to improve this
913 paper, in addition to all of those who made helpful comments on-line or at the symposium. This
914 white paper was updated based on their suggestions.

915

916