

White Paper on Continuous Bioprocessing

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There is a growing interest in realizing the benefits of continuous processing in biologics manufacturing, which is reflected by the significant number of industrial and academic researchers who are actively involved in the development of continuous bioprocessing systems. These efforts are further encouraged by guidance expressed in recent FDA conference presentations. The advantages of continuous manufacturing include sustained operation with consistent product quality, reduced equipment size, high volumetric productivity, streamlined process flow, low process cycle times and reduced capital and operating cost. This technology, however, poses challenges, which need to be addressed before routine implementation is considered. This paper, which is based on the available literature and input from a large number of reviewers, is intended to provide a consensus of the opportunities, technical needs and strategic directions for continuous bioprocessing. The discussion is supported by several examples illustrating various architectures of continuous bioprocessing systems.

Keywords: Continuous bioprocessing, perfusion cell culture, continuous purification, integrated continuous biomanufacturing

1. Introduction

Process intensification through conversion from batch to continuous manufacturing has been applied effectively in industries such as steel casting¹, petrochemical, chemical, food, and pharmaceuticals with great effectiveness.^{2,3,4,5,6} Despite vast differences between the product types, the advantages of continuous over batch manufacturing are consistent and include steady state operation, reduced equipment size, high volumetric productivity, streamlined process flow, low cycle times, and reduced capital cost.⁷ An example of industrial importance in the therapeutic field is the ongoing project at the Novartis - MIT Center for Continuous Manufacturing that targets a holistic redesign of the pharmaceutical manufacturing process to achieve fully integrated end-to-end continuous flow.⁸

There is a growing interest in realizing the benefits of continuous processing in biologics manufacturing. To this end, a significant number of industrial and academic researchers are actively involved in the development of continuous processing systems.^{9,10A} The results reported so far point to the transformative potential of this technology on the manufacturing of biological drugs. The development efforts are further encouraged by guidance expressed in recent FDA conference presentations.^{11,12}

Continuous bioprocessing technology, as a paradigm shift in biologics manufacture, will benefit from standardizing on common terminology, as well as from the alignment of expectations and goals. An objective of this document is to propose such a common understanding and to define strategic directions for further development that will address the current challenges and technological gaps. While the concept of fully continuous bioprocessing will likely face some skepticism, it is important to consider the lengthy but highly successful evolutionary path of the continuous manufacturing in other industries^{1,7}, which is seen today as a “disruptive technology” that moved these businesses to a new level.^{13,14}

2. Definitions

As with other industries, the classification of a biomanufacturing system as continuous depends on the nature of the unit operations and its integration into the final system. Therefore, it is appropriate to first provide a working definition of the term “continuous unit operation”.

A **unit operation is continuous** if it is capable of processing a continuous flow input for prolonged periods of time. A continuous unit operation has minimal internal hold volume. The output can be continuous or discretized in small packets produced in a cyclic manner.

A **process is continuous** if it is composed of integrated (physically connected) continuous unit operations with zero or minimal hold volume in between. To emphasize that all the unit operations are continuous and integrated, such processes are also referred to as **fully continuous** or **end-to-end continuous**. A **process is hybrid** if it is composed of both batch and continuous unit operations.

Continuous processing is a rich technical field that encompasses various concepts, such as flow, systems approach, integration and model-based control. For further discussion of these and other related topics see Badman & Trout.¹⁵

3. Challenges of current biomanufacturing technology and the opportunities offered by continuous processing

The overarching business drivers for accelerated development times and cost control under stringent quality/regulatory requirements continue to dominate the biotechnology industry. At present, biopharma companies often need to flexibly accommodate large-, mid- and small-volume drugs (e.g., niche or orphan drugs), preferably within the same manufacturing facilities. The same is true for therapeutic proteins of different natures, for example stable proteins, such as antibodies, and highly complex (less stable) proteins, such as recombinant enzymes or blood-factors. Furthermore, the ability to rapidly adjust production capacity to accommodate fluctuating and/or mis-forecasted market demands is also needed. Mounting pressure to reduce cost is impacted by growing competition from biosimilar products and by government regulations. As a result, concerns about the long term sustainability and reproducibility of the traditional batch manufacturing facility model with multiple 10-20kL batch bioreactors and downstream trains involving large chromatographic columns have been repeatedly raised. As a consequence of major improvements in upstream product titers and the identification of high potency products, a trend towards the utilization of smaller, possibly single-use bioreactors and purification columns has emerged, which addresses some, but not all, of the limitations with current technology. Below, we enumerate the main challenges of current batch or hybrid biomanufacturing systems, and review the opportunities offered by integrated continuous processing to address these issues.

3.1. Cost

High capital investment costs are associated with traditional stainless steel fed-batch facilities due to larger equipment size and low equipment utilization rates. Continuous processing offers significant opportunity to reduce capital costs through radical reduction of facility and equipment footprints that result from: small bioreactors and chromatography columns; elimination of intermediate hold tanks and non-value-added unit operations; very high volumetric productivity; high equipment utilization rate; single-use technology. The volume of the continuous bioreactors and purification columns can be multi-fold smaller than the corresponding fed-batch equipment due to significantly higher cell density in perfusion systems and the downstream equipment utilization rate. These small footprint facilities can be constructed and commissioned more expediently than traditional large-scale facilities. Additional savings in operating cost are also expected from the improved resin capacity utilization and accompanying decreases in buffer volumes that are offered by continuous chromatography systems. The functionally closed process will require lower environmental class

109 and therefore drive down capital and QC environmental testing costs as well. Other cost savings will
110 occur through an increase in automation and reduction in operator labor. Further improvements in
111 perfusion processes to increase MAb titer through process and media optimization are needed to
112 achieve COG competitive with current fed-batch processes. As media cost is reduced through
113 systemic development, its impact on COG will become less significant.

114 **3.2. Flexibility**

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117 The growing diversity of product pipelines within the industry (including large-volume and small-
118 volume drugs; mAb and non-mAb products) and associated market complexity create a need for
119 production flexibility. Continuous processing offers a significant advantage as it allows rapid capacity
120 adjustments through “numbering up” (addition/removal of parallel production lines) when
121 compared to traditional volumetric scale up. The multi-fold smaller and potentially mobile
122 equipment that is used in continuous processing further enhances this advantage. Another scaling
123 factor in continuous processing is time – the duration of the process can be modulated based on
124 product demand. In combination, these factors allow the utilization of a single bioreactor scale of a
125 few hundred liters for the production of small-volume drugs (<10kg/year) and large-volume drugs
126 (>100kg/year). Furthermore, the reduced equipment footprint and the universality of the platform
127 allows high process mobility and portability, either within the same facility or between different
128 manufacturing sites, which can be strategically distributed to serve local markets.

129 **3.3. Standardization**

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132 The diversity of biological products has resulted in the development of a variety of production
133 systems with limited standardization. For example, relatively stable proteins (such as a MAb) are
134 typically produced in fed-batch systems, while less stable molecules (such as blood factors or
135 enzymes) are produced in hybrid systems (perfusion upstream and batch downstream). There is
136 also significant diversity in production systems even within the same technological category, which
137 complicates knowledge management, technology transfer, speed of development, and the ability to
138 capture incremental process improvement. Continuous bioprocessing offers the opportunity to
139 implement standardization, i.e. all biological drugs are manufactured in a common manner. Multi-
140 product facilities then can be designed using a standardized continuous platform. Furthermore, due
141 to small equipment size, full process standardization can now be realized across process
142 development, clinical production, launch and commercial manufacturing, as identical equipment and
143 control systems can be used in all these areas. Standardization will also facilitate compliance with
144 local government regulations in emerging markets, as small, predesigned facilities can be rapidly and
145 inexpensively built in such regions in a decentralized operating model.

146
147 Furthermore, standard bioreactors of modest volume can be used for the production of both small-
148 volume and large-volume biologics. For example, a single 500L bioreactor operated continuously at
149 cell density of 80e6 cells/mL for a total of 280 days/year would produce more than 400 kg/year at
150 crude harvest, assuming cell specific productivity of 40pg/cell-day. The same 500L perfusion
151 bioreactor can be used in much shorter campaigns for the production of low-volume drugs. By
152 scaling with longer production cycles a range of market demands can be met.

153
154 Additional improvements can be achieved through equipment interchangeability and
155 standardization of interfaces between continuous process equipment. Due to the small, mobile
156 nature of the directly connected continuous unit operations, interface standardization is facilitated
157 by single use technology (e.g., disposable tubing, tubing sealers and tubing welders).

158 **3.4. Speed of scaling**

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161 Historically, scale-up and transfer to manufacturing has been a time consuming activity, often
162 associated with the identification of various technical challenges. The utilization of a standard
163 production platform for protein drugs would facilitate and minimize technology transfer activities.

164 This is achieved by the equivalency of scale and equipment for pilot, clinical, and commercial
165 production. Training and validation would also be faster, as the systems will be well understood and
166 characterized, and proper models can be built and common validation protocols can be used.
167 Equipment cleaning requirements will be reduced. The elimination of non-value unit operations and
168 intermediate hold steps will also have a positive impact on time-to-market. It is clear, however, that
169 such advantages can become more evident with the maturation of the platform, both in terms of
170 technology and regulatory approval procedures.

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172 The physical connection and prolonged uptime of all continuous unit operations during scale-up and
173 validation enable the collection of substantial amounts of data offering an unprecedented
174 opportunity to learn about the bioprocess as an integrated system. Over time, the generation of such
175 deep knowledge will enable faster process development and system deployment. One needs to
176 assure consistency of performance across time, along with an understanding of the minimum scale
177 that make continuous bioprocessing attractive. Production over varying periods of time has to be
178 validated as well to provide additional operational flexibility.

179 180 **3.5. Quality**

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182 Due to extended bioreactor residence time, fed-batch technology is only used for the manufacture of
183 stable proteins. If produced in this mode, labile proteins would either degrade or lose some of their
184 quality attributes. Continuous technology allows a significant decrease of the molecule residence
185 time in the bioreactor, which enables the production of any kind of protein with uncompromised
186 quality. It is worth noting that there may be quality benefits even with the production of stable
187 proteins (e.g. mAb's), as glycosylation profiling changes (less modified and more consistent
188 glycoforms profile) have been reported in batch systems, most likely due to post secretion enzymatic
189 modification or degradation.^{16,17,18} Modifications, such as deamidation, that are associated with
190 prolonged molecule exposure to bioreactor pH and temperature conditions also can be minimized
191 with continuous cultivation. The elimination of intermediate hold steps further reduces the risk of
192 product degradation and eliminates the need of long-term stability studies. Another advantage is
193 that continuous bioreactors typically operate at high cell culture viability, which in turn results in
194 higher productivity, lower impurity levels in the harvest, and potentially simplified product
195 purification schemes. Since the sustained production is done with close attention to process control,
196 this facilitates the application of QbD principles. The high degree of automation associated with
197 continuous processing further increases operational consistency as it minimizes manual operations
198 and subjective decision-making. The upstream and downstream closed system operation needed for
199 long-term continuous runs would further reduce bioburden risk, which is significant in existing
200 downstream facilities.

201 202 203 **4. Technology needs**

204 205 **4.1. Different requirements for upstream and downstream**

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207 Continuous perfusion bioreactors have been employed for decades for the commercial manufacture
208 of biologics. In these "hybrid" systems, the bioreactor equipped with a cell retention device is the
209 only continuous unit operation. The downstream part of the process consists of multiple batch unit
210 operations. While significant knowledge with continuous bioreactor operation has been
211 accumulated over the years, the experience with continuous downstream operations is limited. Due
212 to the different levels of maturity, technological needs for upstream and downstream development
213 are rather different.

214
215 Technology evolution in a continuous upstream system is expected to be incremental within the
216 existing process architecture. The established bioreactor-cell retention device configuration offers
217 significant advantages, and will likely remain conceptually the same. Improvements within this
218 framework are, however, necessary in order to reach the full potential of the continuous platform.

219 These include the development of robust and stable cell lines that maintain high productivity over
220 prolonged time periods (e.g., 2-3 months), the design of media formulations to support high cell
221 density (e.g., capable of supporting >50e6 cells/mL at perfusion rate of 1-2 reactor vol/day), as well
222 as optimization of bioreactor conditions to provide the high cell density at high viability and positive
223 growth rate. Various enabling technologies need to be developed and optimized, such as automatic
224 cell density control, efficient oxygenation and ventilation, foam control, etc. As bioreactor operation
225 at cell densities above 100e6 cells/mL has already been demonstrated¹⁹, achieving these targets at
226 industrial scale within the continuous upstream technological infrastructure is a realistic near term
227 goal.

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229 The current situation with downstream is quite different, as there is limited experience with
230 continuous protein purification, especially at manufacturing scale. Until recently, equipment for
231 continuous protein purification operations was not available. Today, small- and pilot-scale
232 continuous chromatography systems are offered by several equipment manufacturers (Novasep,
233 Pompey, France; Tarpon, Worcester, MA; Semba, Madison, WI; GE Healthcare, Piscataway, NJ;
234 Knauer, Berlin, Germany; ChromaCon, Zurich, Switzerland). As these systems are new, their
235 adoption by the biotechnology community as routine tools will take time to evaluate, validate and
236 implement. Significant experience needs to be accumulated in process scale up prior to adoption at
237 full scale. Most unit operations employ multicolumn technology utilizing time- or UV-based switching
238 logic that enables the system to automatically process continuous flow. Other, less mature
239 technologies also may be considered, such as annular chromatography²⁰ or Continuous
240 Countercurrent Tangential Chromatography.²¹ In addition to the chromatography steps, novel
241 downstream unit operations are needed, such as continuous viral inactivation/removal and UF/DF,
242 among others. An important design requirement for all continuous downstream unit operations is
243 their ability to operate over prolonged periods under stringent bioburden control conditions.

244
245 A major lesson from the development of continuous processes in pharmaceuticals and other
246 industries is that one does not convert a batch process to continuous by simply connecting together
247 existing batch equipment, but rather by designing new fit-for-purpose unit operations and processes.
248 This places a strong dependence on the technology suppliers. There must be broad support by the
249 technology vendors, who have to develop the equipment suitable for commercial continuous
250 processing.

251 252 **4.2. Standardization of downstream process architecture**

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254 Additional challenges emerge with standardization of the downstream process architecture. While
255 the purification of mAbs is relatively well defined, (e.g. protein-A capture), this is not the case with
256 non-mAb molecules. The batch purification trains vary significantly in number and type of
257 chromatography columns, viral inactivation methods, deployment of membrane steps and final
258 formulation. One possible avenue towards the development of a universal downstream architecture
259 is the rational design of highly specific ligands for the capture step analogous to Protein A in mAb
260 purification. While so far this approach has been challenging, the availability of such robust and
261 specific ligands will help standardize the remaining downstream unit operations, ideally utilizing no
262 more than three chromatographic steps.

263
264 As today's continuous downstream unit operations are in a relatively early phase of development,
265 one can expect hybrid versions to first be established before fully continuous production systems
266 emerge. In these systems, the continuous portion may include a perfusion bioreactor integrated with
267 a continuous capture step. As experience grows and new enabling technologies are developed,
268 subsequent downstream unit operations can be converted to continuous and integrated into the
269 system.

270 271 **4.3. Further optimization of cell culture media**

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273 The upstream operational expenses are closely related to the amount and cost of the cell culture
274 media. A strategic need is the development of highly nutritional medium formulation capable of
275 supporting very high cell densities (>50e6 cells/mL) at low volumetric perfusion rates (1-2
276 bioreactor vol/day). This decreased media consumption, paralleled with low media cost per liter,
277 would result in competitive upstream operational expenses. An obvious prerequisite in the medium
278 optimization efforts is the maintenance of high cell viability and productivity, and consistent product
279 quality during the entire course of the continuous cultivation.

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281 **4.4. Global process control**

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283 Unit operations are typically designed as autonomous systems equipped with their own local
284 controls. Such local control is sufficient in batch processing, as the unit operations are disconnected
285 and do not need information from each other in order to function properly. While local control is
286 also essential in continuous processing, the integration of unit operations requires global
287 coordination of the entire process flow. Consequently, continuous systems have to be equipped with
288 a second level software control system that supervises and aligns the work of the individual unit
289 operations. Typical oversight functions are coordination of flow rates, event-based control and
290 exception handling. The software and hardware system should provide a high degree of automation,
291 requiring minimal operator involvement. A potential challenge here is that different vendors often
292 use different control systems, which can make such kind of integration difficult. Standards for
293 aligning local and global control will facilitate continuous operation.

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295 **4.5. Process Analytical Technology (PAT)**

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297 Tightly associated with process automation and control is the need for adequate PAT. Reliable long-
298 term operation of the continuous system can be accomplished if adequate real-time information is
299 available for each unit operation. To a significant extent this has been achieved for bioreactor
300 operation, as demonstrated by the successful multi-month operation of existing commercial
301 perfusion processes. Physical and physico-chemical parameters are reliably monitored in
302 continuous chromatography systems (e.g., UV absorbance, pH, conductivity, flow rate, pressure, etc.)
303 using technologies that are well established in batch processes. What is missing, however, is
304 sufficient amount of real-time information about product quality attributes (activity, aggregation,
305 glycosylation, impurity level, etc.). Development of PAT that addresses this need will be of
306 tremendous importance. Since this is a task of high complexity, reliable on-line sensor solutions are
307 unlikely to emerge in the near term. A more realistic option is the implementation of approaches
308 based on sterile sampling and at-line rapid analysis using established instrumentation. Such systems
309 can be positioned at several strategic points along the process flow, and can work in “quasi real-
310 time”, supplying control systems with the required product quality information. In any case, the
311 progress in this area is expected to be incremental, reflecting the ever improving capability of the
312 analytical technology.

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314 **4.6 Single Use Technology**

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316 The majority of end users consider the further expansion of capacity from a “facility of the future”
317 standpoint to be based upon single-use closed technology, regardless of the mode of operation (batch
318 or continuous). As the key benefits of single-use, such as low capital cost, low downtime and flexible
319 footprint, are similar to these provided by continuous processing, there is a strong synergy between
320 these two technologies. With improvement in upstream productivity, systems may be smaller,
321 further benefiting single-use technology. Therefore, single use technology is often seen as an enabler
322 for continuous closed processing, including both up- and down-stream operations. While single use
323 technology has made an impressive progress over the last several years, there are still significant
324 needs for alignment between suppliers and end users on key issues, such as GMP regulatory
325 requirements, need for standardization in E&L testing procedures, standards for bag/tubing
326 manifold systems, lack of robust ON/OFF sterile connectors, etc. Addressing these issues will

327 accelerate and expand single use implementation and ultimately reduce the nervousness of
328 continuous processing implementation.

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331 **5. Issues to be addressed**

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333 As with any new technology, continuous bioprocessing is not yet mature and requires sustained
334 innovation and guided evolution in terms of methodology and technology. Here, we review several
335 high-impact areas that need particular attention.

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337 **5.1. Regulatory roadmap**

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339 While there is significant experience with continuous perfusion systems, a partial or complete
340 integration between upstream and downstream has not yet been commercially demonstrated. The
341 impressive successes of continuous flow processing in the pharmaceutical industry have attracted
342 the attention of the regulatory authorities, who are increasingly supportive of this new
343 manufacturing paradigm. FDA has recently provided comments about the applicability of continuous
344 manufacture of synthetic drugs with highly encouraging conclusions.²² As the parallels to biotech are
345 obvious, these discussions provide a framework and path to address potential regulatory hurdles for
346 implementation of the novel continuous bioprocessing paradigm. In order for companies to be
347 sufficiently motivated to move towards continuous technology, it is important that the regulatory
348 path does not impose unrealistic challenges that would counterbalance the discussed technological
349 benefits. As industrial and regulatory experience grows, the path to approval is expected to become
350 simpler and shorter.

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352 Most recently, a presentation focusing specifically on continuous biomanufacturing was delivered by
353 the FDA.¹² The key conclusions were in line with previous guidance in the context of small molecule
354 drugs. The main take home messages are that there is “nothing in regulations or guidance
355 prohibiting continuous manufacturing,” and “continuous manufacturing is fully consistent with FDA’s
356 QbD in which envelopes of performance are seen as part of the control strategy.” There is clarity that
357 lot sizes may be determined by either mass or time. The regulatory expectations for assurance of
358 reliable and predictive processing in a commercial setting are the same for batch and continuous
359 processing.

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361 **5.2. Challenges to adoption**

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363 According to Reay² the reasons for the relatively slow penetration of new processing methodologies
364 include, low tolerance of risk, management concerns about implementing new technologies,
365 overinvestment in existing facilities designed for the old principles, the legacy effect of fully
366 depreciated production plants and, not the least, perceived regulatory constraints. While these
367 impediments to change are particularly strong in the field of biopharmaceuticals, where there is a
368 relationship between the process and the product, the evolving competitive business environment
369 and desire to address global markets is incrementally driving the biotech industry towards a tipping
370 point where existing barriers may be counterbalanced by the need for radically improved
371 bioprocessing. In all cases, the success of the introduction of innovative approaches depends not
372 only on sound technical vision, but also on broad support from the entire organization as a matter of
373 corporate strategy.^{23,7}

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375 Well-founded or not, process related concerns include those regarding start-up and shutdown
376 material losses and costs, long validation times, ability to achieve robust process throughput, fears
377 that equipment cleaning may be more difficult or complicated, and the perception that when any unit
378 operation in continuous processing is down for any reason, the whole process is down.²⁴

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380 Most importantly, the adoption of continuous processing is facing the challenge of the deeply
381 entrenched “batch technology mindset,” which penetrates organizations at all levels. The

382 implementation of a new technology cannot be a bottom-up initiative, and the complete support of
383 top management is essential. To this end, a strategic vision backed by a convincing business case and
384 solid development scale data needs to be prepared with broad consensus; this is particularly
385 important for the early adopters. Careful selection of the product for the first implementation of a
386 new technology is essential, as concerns about extending the time-to-market may play a critical role
387 in technology selection.

388 **5.3. Supply chain considerations**

389 It is known from other industries, such as food and chemicals, where continuous processing has been
390 applied for a long time, that there is an increased dependence on quality and consistency of raw
391 material in the supply chain. This is essential in order to minimize variance going into the process. If
392 single-use technologies are incorporated into the process, there is greater dependency on technology
393 vendors. In these cases, extra rigor in quality assurance will be required because it takes on
394 additional importance.

395 Continuous operation also has the potential to positively influence the downstream side of the supply
396 chain, as there is greater flexibility in meeting variable demands from the market since scaling is by
397 time extension and not by the scale of batches. This is further enhanced by the short process cycle
398 time and the opportunity to reduce inventories at hands. Demand may also be met by the mobility of
399 smaller production systems and the opportunity to decentralize production and distribute
400 manufacturing locally closer to markets.

401 **5.4. Impact on business strategy**

402 There is a significant positive impact on the business strategy that is enabled by the increase in
403 flexibility, shortened scale-up and process development time, standardization and reduced capital
404 requirements for an operating plant. The flexibility will permit a more responsive supply chain that
405 is especially important in new and uncertain markets. The lower capital costs may enable smaller
406 companies to integrate manufacturing earlier in their life-cycle and reduce the dependence on CMOs.
407 With smaller plants that can be scaled by time rather than volume, the same facility can be used for
408 clinical material manufacturing and product launch (i.e., multi-purpose facilities). Market growth can
409 be accommodated by longer production cycles or installation of identical parallel process trains.
410 With a standard production platform, the same unit may be used for multiple products, which further
411 increases operational flexibility and cost structure.

412 **5.5. Impact on organizational structure**

413 Accommodation of continuous production will likely require changes in organizational structure.
414 Upstream and downstream distinctions will blur as the bioreactor and chromatography steps
415 become integrated unit operations of one continuous stream. This will have implications on the
416 development and manufacturing organization that will also need to be integrated across the process.
417 These structural modifications will require a change in the culture of the organization. Operational
418 excellence will require compliance under sustained and continuous operation, with an emphasis on
419 process control. Longitudinal data will be collected and new methods for learning will need to
420 emerge.

421 **6. Examples**

422 The potential for, and experience with, continuous processing is illustrated with several examples
423 drawn from recent literature on therapeutic protein manufacturing using mammalian cell culture.
424 The four process architectures (Fig. 1-4) are idealized to illustrate each approach and do not try to
425 capture all the technical details. The examples include three hybrid systems and one fully integrated
426 system.

436 continuous process. All cases demonstrate the advantages of continuous processing, with the fully
437 continuous system offering the strongest potential.

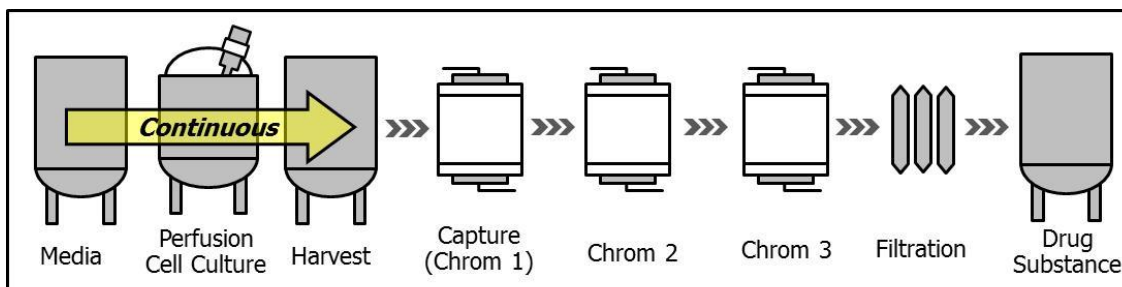
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6.1. Hybrid system: Continuous upstream with batch downstream

441 The process architecture in Fig. 1 is widely used today for commercial manufacturing of
442 complex/labile proteins, such as enzymes, blood factors and, in some cases, mAbs. Over the last 25
443 years, several companies, including Genzyme, Bayer, Janssen, BioMarin, Shire, Merck-Serono,
444 Novartis and Pfizer, have practiced perfusion culture. The bioreactor residence time of the product is
445 short, usually <24hrs, which enables the production of unstable proteins with minimal degradation.
446 The harvest is collected in large tanks, and processed downstream in a traditional batch fashion,
447 starting with clarification for cell removal and a capture step. The utilization of filtration based cell
448 retention devices, such as ATF or TFF, enables integration of bioreactor operation and clarification
449 into a single unit process.^{25,26,19, 27} Pollock at al.²⁷ have illustrated how the economic competitiveness
450 of bioprocesses employing perfusion culture depends on cell density increase that is achievable in
451 perfusion systems.

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This process configuration allows utilization of small and even mobile bioreactors in the upstream production suite. However, the batch downstream operation still requires large equipment, which minimizes some of the benefit accrued in the continuous upstream design. Nevertheless, perfusion cell culture has been of tremendous use to the biotechnology community because it has enabled the production of unstable proteins, which is difficult or impossible to accomplish with traditional fed-batch technology.

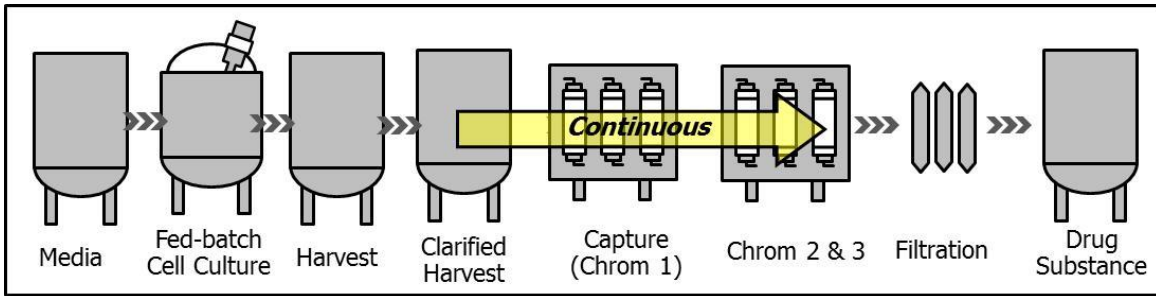


Example 1: Continuous upstream (perfusion), batch downstream

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6.2. Hybrid system: Batch upstream with continuous downstream

This process architecture has been recently explored at development and pilot scale (Fig. 2). The cells are cultured in traditional fed-batch mode, while one or more of the downstream unit operations are converted into continuous operation. Various continuous unit operations are being developed, such as precipitation²⁸, flow-through purification²⁹, directly coupled chromatography columns without hold vessels in between³⁰ and viral inactivation³¹. In most of these cases, the continuity of the downstream operation is defined within the limits of a single upstream batch on a mass basis. This mode of operation has been shown to be economically beneficial.³² For example, the much smaller volume of continuous chromatography columns results in significant savings when expensive chromatography resins are used (e.g, Protein A). Bioprocesses utilizing continuous chromatography for product capture offer significant direct cost savings in clinical material production, which can have a large impact considering the high clinical attrition rates.³²

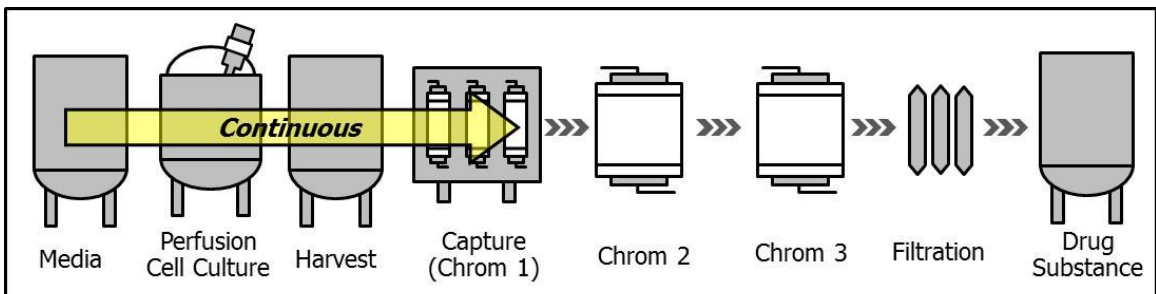


Example 2: Batch upstream, continuous downstream

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6.3. Hybrid system: Continuous bioreactor and capture followed by batch (post-capture) downstream

In this model, the continuous processing extends downstream of the bioreactor to include the capture step, as shown in Fig. 3. This integration is considered particularly advantageous for two reasons. First, is the elimination of large hold tankage (including clarification unit operations) between the bioreactor and the capture step. Second, the implementation of continuous capture results in 1-2 orders of magnitude reduction in column size and lowers buffer utilization, which is particularly important when the capture step employs columns of large diameter. Various versions of Simulated Moving Bed (SMB) multicolumn systems are being used for the implementation of the continuous capture step. An example of this approach for the production of a recombinant enzyme and mAb is described by Warikoo et al.³³ A 3-column continuous chromatography system was integrated with a high cell density perfusion bioreactor. The system was successfully run for a period of two months, and achieved steady state operation with respect to product quality.



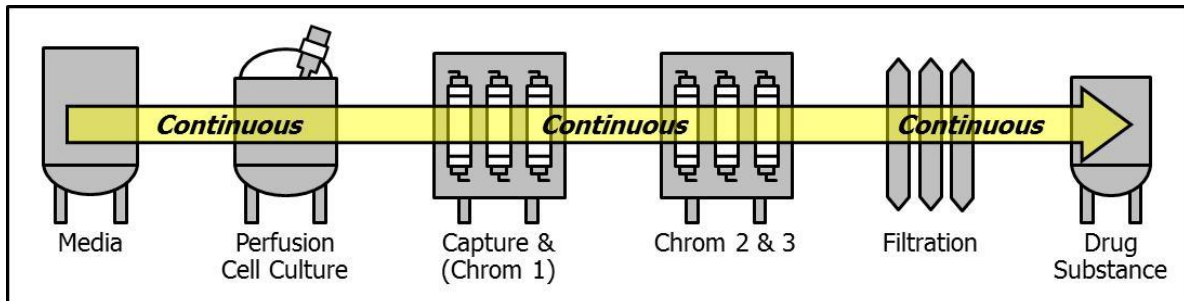
Example 3: Continuous upstream + capture, batch downstream

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6.4. Fully integrated continuous process

This process configuration consists of fully integrated continuous unit operations for the entire process train (Fig. 4). Development scale examples of such systems have been presented recently.^{34,35} The fully integrated continuous process offers impressive advantages, such as small equipment footprint, low residence and cycle times, and low cost. However, not all unit operations required for the implementation of such a system are commercially available at scale today. Additional efforts are required to establish robust viral inactivation or removal systems that operate continuously at operating scale. The same applies to the UF/DF step at the downstream process. The direct coupling of the individual unit operation requires compatibility of their interfaces, which points to a generic need to focus on interfaces between unit operations. The single-use technology

508 offers advantages in this respect because of the utilization of weldable plastic tubing of various
509 diameters.
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Example 4: Continuous upstream and downstream

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7. Recommendations

Continuous processing offers exciting new opportunities for improving the manufacture of biological products. For this technology to be successfully implemented, the joint efforts of industry, academia, regulatory authorities and equipment vendors are needed. Below are a few recommendations that will help to address the existing technical and non-technical challenges:

- 521 • Knowledge and learning. The impact of continuous bioprocessing will evolve from the collective
522 action of academic and industrial researchers, via knowledge sharing on systems and their
523 performance as well as ongoing evaluation of innovative ideas. It is recommended that there be
524 a regular forum for bringing together the academic, industrial and regulatory community to
525 review results, propose new technologies, and promote discussions on development and
526 deployment of continuous bioprocessing. Examples of such events are the biannual Integrated
527 Continuous Biomanufacturing Conference (Oct 20-24, 2013, Barcelona) and the International
528 Symposium on Continuous Manufacturing of Pharmaceuticals (May 20-21, 2014; MIT-
529 Cambridge, USA). Workshops between industry and FDA/EMA will also help guide industry
530 during the early phases of development and implementation of this new technology.
- 531 • Equipment vendors play a key role in the development and implementation of continuous
532 technology. Industry-vendor forums need to be established to define the requirements for
533 continuous biomanufacturing unit operation (longevity, closed systems, sterility) and the
534 interfaces between them.
- 535 • There are several mission critical requirements for production of safe and efficacious biologic
536 products that include viral clearance, in-process testing, supply chain audit, etc. that will be
537 different for batch and continuous bioprocessing. These activities need to be addressed through
538 research in an open forum so that manufacturers and equipment vendors can bring forward the
539 best processes for therapeutic products.
- 540 • There is an important role for government in addressing the related issues. Cooperation
541 between FDA and industry to develop a road-map for the implementation of continuous
542 bioprocessing will be highly beneficial. Government funding of related research in academia will
543 accelerate progress in the field. An example is the provision of certain incentives to
544 equipment/instrumentation vendors to develop required continuous unit operations
545 (particularly downstream) and PAT instrumentation.
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- Industry-academia collaborations in continuous bioprocessing (such as the Novartis-MIT alliance) will enable sharing of risk and cost, and may be established perhaps in the form of academia-industry consortia to develop, for example, common unit operations and platforms.

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